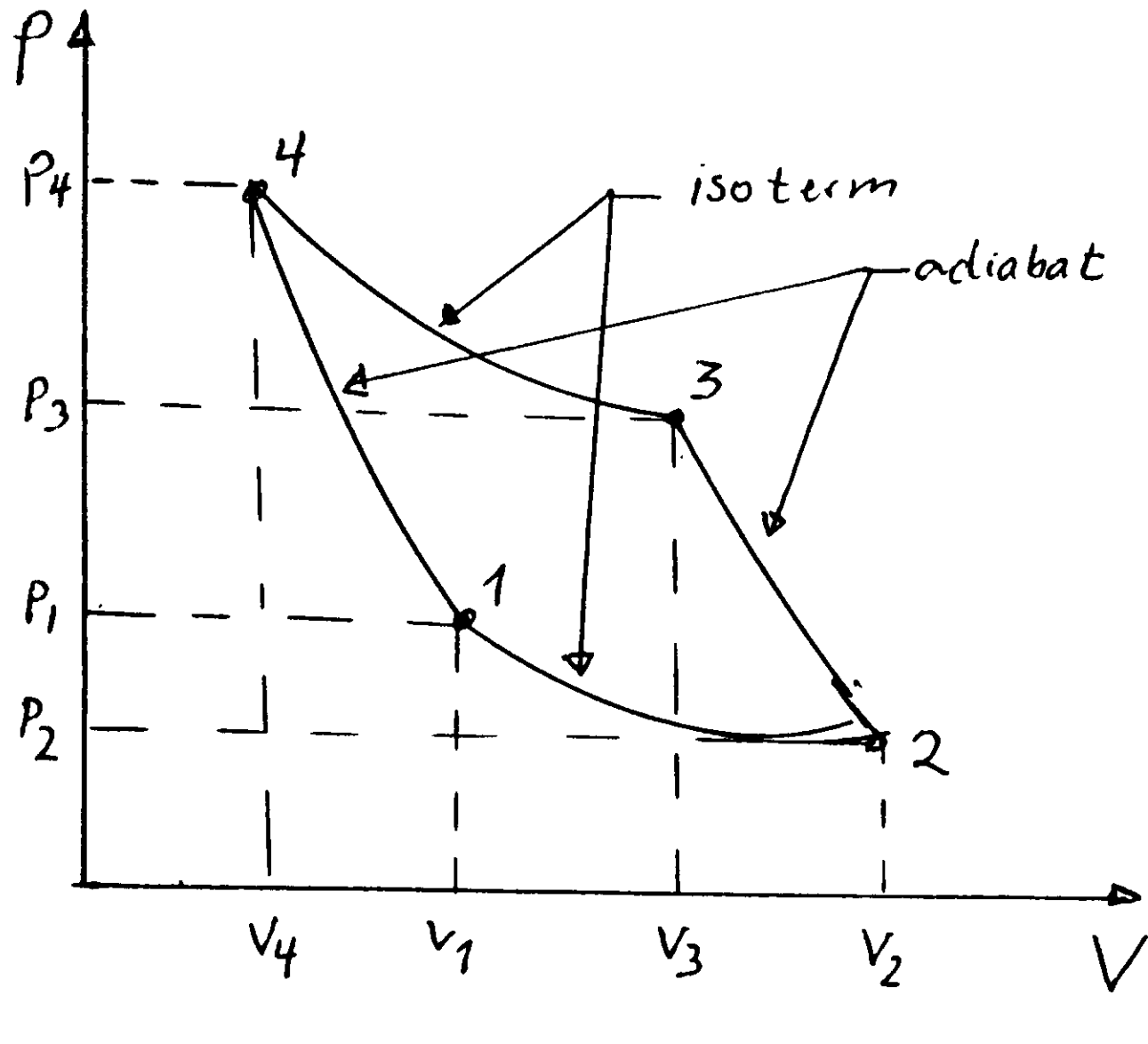


LØSNINGSFORSLAG

Oppgave 1

a)



Gasslign.: $pV = nRT$

$$\underline{\underline{m = \frac{p_1 V_1}{RT_1}}}$$

b) Isotherm; $\Delta U = 0 \Rightarrow$

$$Q_1 = W_{12} = \int_{V_1}^{V_2} p dV = mRT_1 \int_{V_1}^{V_2} \frac{dV}{V} = mRT_1 \ln\left(\frac{V_2}{V_1}\right) = \underline{\underline{p_1 V_1 \ln\left(\frac{V_2}{V_1}\right)}}$$

$$Q_3 = W_{34} = \int_{V_3}^{V_4} p dV = mRT_3 \ln\left(\frac{V_4}{V_3}\right) = \underline{\underline{p_1 V_1 \frac{T_3}{T_1} \ln\left(\frac{V_4}{V_3}\right)}}$$

V_i kan $W_{23} = -W_{41} \Rightarrow$ Totalt tilført arbeid:

$$W = W_{12} + W_{34} = p_1 V_1 \left[\ln\left(\frac{V_2}{V_1}\right) + \frac{T_3}{T_1} \ln\left(\frac{V_4}{V_3}\right) \right]$$

c) Pumpens effektivitet:

$$\epsilon = \frac{Q_3}{W} = \frac{p_1 V_1 \frac{T_3}{T_1} \ln\left(\frac{V_4}{V_3}\right)}{p_1 V_1 \left[\ln\left(\frac{V_2}{V_1}\right) + \frac{T_3}{T_1} \ln\left(\frac{V_4}{V_3}\right) \right]} = \frac{T_3 \ln\left(\frac{V_4}{V_3}\right)}{T_1 \ln\left(\frac{V_2}{V_1}\right) + T_3 \ln\left(\frac{V_4}{V_3}\right)} \quad *)$$

V_i kan:

$$\left. \begin{aligned} T_1 V_2^{\gamma-1} &= T_3 V_3^{\gamma-1} \\ T_3 V_4^{\gamma-1} &= T_1 V_1^{\gamma-1} \end{aligned} \right\} \frac{T_1 V_2^{\gamma-1}}{T_1 V_1^{\gamma-1}} = \frac{T_3 V_3^{\gamma-1}}{T_3 V_4^{\gamma-1}}$$

$\Rightarrow \frac{V_2}{V_1} = \frac{V_3}{V_4}$ innsett i lign. *):

$$\epsilon = \frac{T_3 \ln\left(\frac{V_1}{V_2}\right)}{T_1 \ln\left(\frac{V_2}{V_1}\right) + T_3 \ln\left(\frac{V_1}{V_2}\right)} = \frac{T_3 \ln\left(\frac{V_1}{V_2}\right)}{T_3 \ln\left(\frac{V_1}{V_2}\right) - T_1 \ln\left(\frac{V_1}{V_2}\right)} = \frac{T_3}{T_3 - T_1}$$

d) Reell virkningsgrad:

$$\epsilon_r = 0,55 \cdot \epsilon = 0,55 \frac{T_3}{T_3 - T_1} = 0,55 \frac{343}{343 - 280} = \underline{\underline{3,0}}$$

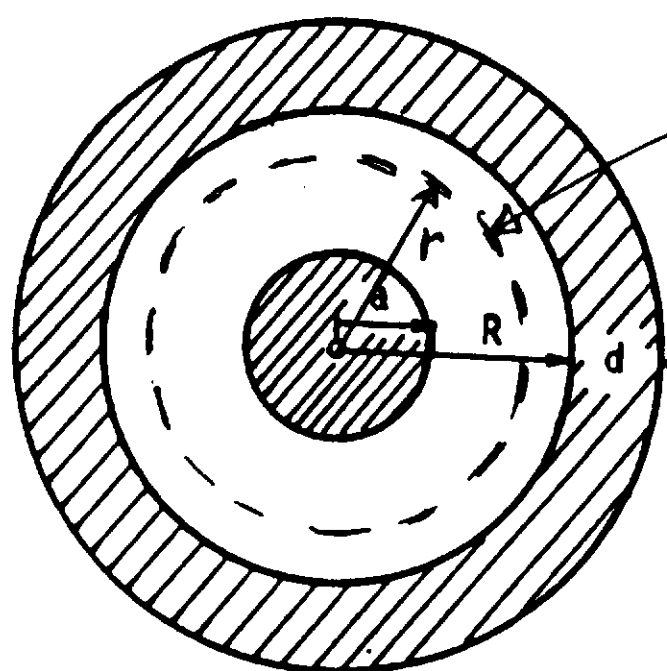
Sentralvarmeanlegget mottar effektivest P som er 90% av pumpens angitte effekt P_3 .

$$P_3 = \frac{P}{0,9} = \frac{1,8 \cdot 10^7}{0,9} \text{ W} = \underline{\underline{2 \cdot 10^7 \text{ W}}}$$

$$\epsilon_r = \frac{P_3}{P_0} = \frac{P}{0,9 \cdot P_0} = 3$$

$$\Rightarrow P_0 = \frac{P}{3 \cdot 0,9} = \frac{1,8 \cdot 10^7}{2,7} \text{ W} = \frac{2}{3} \cdot 10^7 \text{ W} = \underline{\underline{0,67 \cdot 10^7 \text{ W}}}$$

$$\epsilon_{\text{sys}} = \frac{P}{P_0} = \frac{3 \cdot 1,8 \cdot 10^7}{2 \cdot 10^7} = \underline{\underline{2,7}}$$

Oppgave 2

Gauss-flate: Sylinder
med radius r og lengde l

Gauss sets:

$$\oint \vec{E} d\vec{A} = \frac{q}{\epsilon_0}$$

a) i) $a < r < R$

$$\oint \vec{E} d\vec{A} = E(r) \int dA = E(r) \cdot 2\pi r l = \frac{\lambda_1 l}{\epsilon_0}$$

$$\Rightarrow E(r) = \underline{\underline{\frac{\lambda_1}{2\pi\epsilon_0 r}}}$$

ii) $r > R+d$

$$E(r) \cdot 2\pi r \cdot l = \frac{(\lambda_1 + \lambda_2) l}{\epsilon_0}$$

$$\Rightarrow E(r) = \underline{\underline{\frac{\lambda_1 + \lambda_2}{2\pi\epsilon_0 r}}}$$

b) i) I et metall må det elektriske feltet være lik null. I motsatt fall har vi en strøm i ledningen

ii) Lading pr. meter i indre cylindervegg = λ_2^{indre}
 ——— || ——— ytre ——— || ——— = λ_2^{ytre}

Gauss-flaten ligger i ytre cylinder.
 Da ladingen fordeles seg på cylinderveggene gir Gauss sats:

$$E(r) \cdot 2\pi r l = \frac{(\lambda_1 + \lambda_2^{indre}) l}{\epsilon}$$

For at $E(r) = 0$, må vi ha:

$$\underline{\underline{\lambda_2^{indre} = -\lambda_1}}$$

$$\lambda_2^{ytre} = \lambda_2 - \lambda_2^{indre} = \underline{\underline{\lambda_2 + \lambda_1}}$$

c) Amperes lov $\oint \vec{B} d\vec{l} = \mu I$

i) $r < a$

$$\oint \vec{B} d\vec{l} = B(r) \oint dl = B(r) \cdot 2\pi r = \mu r \cdot i_1 \frac{r^2}{a^2}$$

$$\Rightarrow \underline{\underline{B(r) = \frac{\mu r i_1}{2\pi} \frac{r}{a^2}}}$$

ii) $a < r < R$

$$B \cdot 2\pi r = \mu_0 i_1$$

$$\Rightarrow \underline{\underline{B(r) = \frac{\mu_0 i_1}{2\pi r}}}$$

iii) $r > R + d$

$$B(r) \cdot 2\pi r = \mu_0 (i_1 + i_2)$$

$$\Rightarrow \underline{\underline{B(r) = \frac{\mu_0 (i_1 + i_2)}{2\pi r}}}$$

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iv) Brøkdelen av strømmen i_2 innefor
søyfa med radius r er:

$$\frac{r^2 - R^2}{(R+d)^2 - R^2}$$

$$R < r < R+d$$

$$\underline{\underline{B(r) = \frac{\mu_0}{2\pi r} \left(i_1 + i_2 \frac{r^2 - R^2}{(R+d)^2 - R^2} \right)}}$$

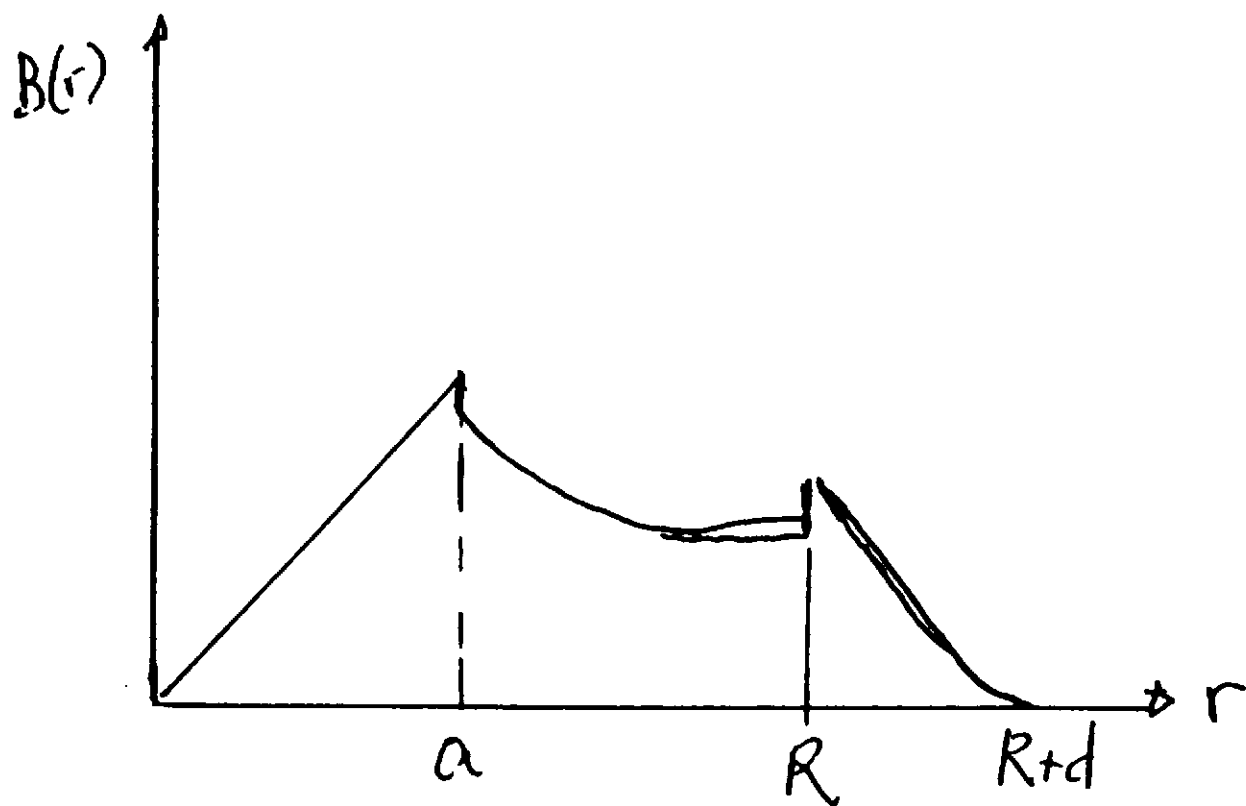
For $i_1 = -i_2$:

$$r < a : B(r) = \frac{\mu_0 i_1}{2\pi a^2} r$$

$$a < r < R : B(r) = \frac{\mu_0 i_1}{2\pi} \frac{1}{r}$$

$$R < r < R+d : B(r) = \frac{\mu_0 i_1}{2\pi r} \left(1 - \frac{r^2 - R^2}{(R+d)^2 - R^2} \right)$$

$$r > R+d : B(r) = 0$$

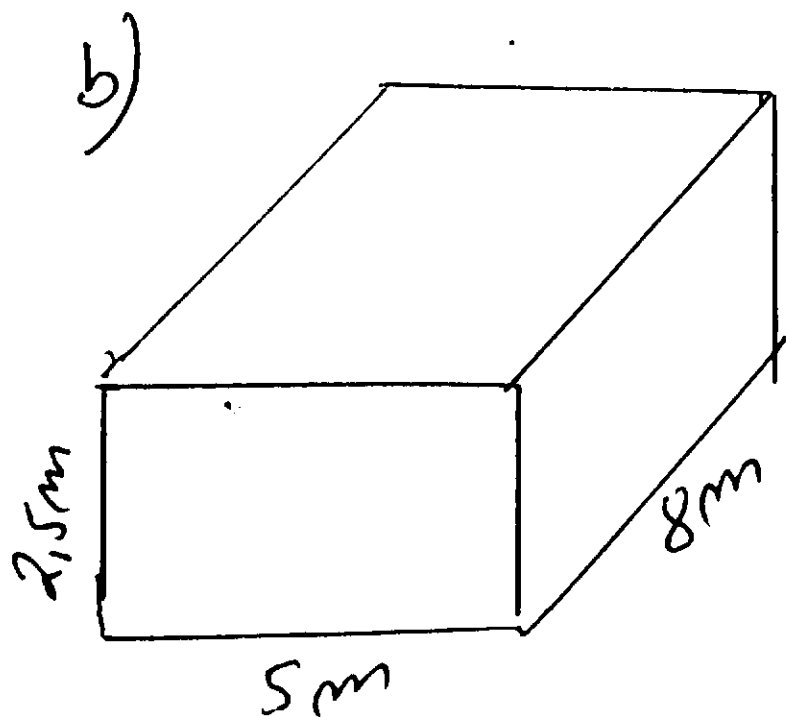


Oppgave 3

a) Varmekledning: $j_e = \lambda \frac{T_2 - T_1}{d}$
 Varmestråling: $j_s = \sigma (T_2^4 - T_1^4) \approx 4\sigma T_1^3 (T_2 - T_1)$

$$j_e = 0,024 \frac{290 - 265}{0,012} = \underline{\underline{50 \text{ W/m}^2}}$$

$$j_s = 5,67 \cdot 10^{-8} (290^4 - 265^4) = \underline{\underline{121,4 \text{ W/m}^2}}$$



Veggareal: $26\text{m} \times 2,5\text{m} = 65\text{m}^2$
 Gulvtak: $2 \times 5 \times 8\text{m}^2 = 80\text{m}^2$

Vindusareal: 10% av $65\text{m}^2 = 6,5\text{m}^2$

\Rightarrow Veggareal = $58,5\text{m}^2$

Varmetap pr. m^2 i vegg/tak:

$$j_e = \frac{T_2 - T_1}{\frac{b_1}{d_1} + \frac{b_2}{\lambda_2} + \frac{b_1}{\lambda_1}} = \frac{290 - 265}{\frac{2,5 \cdot 10^{-2}}{0,14} + \frac{0,15}{0,047} + \frac{2,5 \cdot 10^{-2}}{0,14}}$$

$$= \frac{25}{3,548} = \underline{\underline{7,046 \text{ W/m}^2}}$$

Totalt tap vegg/tak:

$$J_{VT} = j_e \times \text{areal} = 7,046 \cdot (80 + 58,5) = 975,9 \text{ W}$$

Totalt tap vinduer:

$$J_v = (j_{gs} + j_e) \times \text{areal} = (12,4 + 50) \cdot 6,5 = 1114,1 \text{ W}$$

$$J_{\text{total}} = J_{VT} + J_v = 975,9 + 1114,1 = 2090 \text{ W}$$

Brøkdelen vindustap: $\frac{1114,1}{2090} = \underline{\underline{53,3\%}}$

c) Inkluderer tap vegg/luft:

$$j_e = \frac{T_2 - T_1}{\frac{b_1}{\lambda_1} + \frac{b_2}{\lambda_2} + \frac{b_1}{\lambda_1} + \frac{2}{h}} = \frac{25}{3,548 + 0,2} = 6,67 \text{ W/m}^2$$

Reduksjon i varmestremstetthet:

$$7,046 - 6,670 = \underline{\underline{0,376 \text{ W/m}^2}}$$

som i % blir $\frac{0,376}{7,046} = 0,053 \Rightarrow \underline{\underline{5,3\%}}$

d) Varmestrøm i venstre mellemrum:

$$j_1 = 4\sigma \bar{T}_m^3 (\bar{T}_m - \bar{T}_1) + \frac{\bar{T}_m - \bar{T}_1}{d/\lambda}$$

$$= \left(4\sigma \bar{T}_m^3 + \frac{\lambda}{d}\right) (\bar{T}_m - \bar{T}_1)$$

Varmestrøm i højre mellemrum:

$$j_2 = 4\sigma \bar{T}_m^3 (\bar{T}_2 - \bar{T}_m) + \frac{\bar{T}_2 - \bar{T}_m}{d/\lambda}$$

$$= \left(4\sigma \bar{T}_m^3 + \frac{\lambda}{d}\right) (\bar{T}_2 - \bar{T}_m)$$

Ved lighederet er $j_1 = j_2 \Rightarrow \bar{T}_m - \bar{T}_1 = \bar{T}_2 - \bar{T}_m$

$$\Rightarrow \underline{\underline{\bar{T}_m = \frac{\bar{T}_1 + \bar{T}_2}{2}}} \quad \text{g.v.d.}$$

Varmestrømtæthed, stråling:

$$j_s = \sigma (\bar{T}_2^4 - \bar{T}_m^4) \approx 4\sigma \bar{T}_2^3 (\bar{T}_2 - \bar{T}_m) = 4\sigma \bar{T}_2^3 \left(\bar{T}_2 - \frac{\bar{T}_1 + \bar{T}_2}{2}\right)$$

$$= 4\sigma \bar{T}_2^3 \left(\frac{\bar{T}_2 - \bar{T}_1}{2}\right)$$

Dette er halvdelen af strømtætheden vi ville fåt med dobbeltvindu. Altså

$$j_s = \frac{121,4}{2} \text{ W/m}^2 = \underline{\underline{60,7 \text{ W/m}^2}}$$

Varmestrøm ved ledning blir å regne som om det midterste vindu var borte (p.g.a. at glasset er en god leder sammenlignet med luft)

$$j_e = \lambda \frac{\bar{T}_2 - \bar{T}_1}{d} = 0,024 \frac{290 - 265}{0,020} = \underline{\underline{30 \text{ W/m}^2}}$$

$$\text{Totalt: } j = j_s + j_e = 60,7 + 30 = \underline{\underline{90,7 \text{ W/m}^2}}$$